



Short communication

Ether-based electrolyte enabled Na/FeS₂ rechargeable batteries

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ABSTRACT

We demonstrate for the first time that by simply substituting ether-based electrolyte (1.0 M NaCF₃SO₃ in diglyme) for the commonly used carbonate-based electrolyte, the cyclability of FeS₂ towards sodium storage can be significantly improved. A sodiation capacity over 600 mAh/g and a discharge energy density higher than 750 Wh/kg are obtained for FeS₂ at 20 mA/g. When tested at 60 mA/g, FeS₂ presents a sodiation capacity of 530 mAh/g and retains 450 mAh/g after 100 cycles, much better than the cycling performance of Na/FeS₂ tested in carbonate-based electrolyte.

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1. Introduction

Recently, sodium ion batteries have been realized as an alternative to lithium ion batteries for large-scale energy storage applications due to the low cost of sodium [1,2]. In recent years, various high capacity anode materials have been developed for sodium ion batteries [3–8]. However, on the cathode side, the capacity is often low (<200 mAh/g), mainly due to the intrinsic limit of intercalation-type cathodes, which can only accommodate one Na⁺ per transition metal core [9]. Alternative chemistries with higher capacities arise from conversion-reaction type materials, benefiting from their ability of accommodating more than one sodium ion per transition metal core. Among all conversion-reaction type materials, FeS₂, which is a well-known semiconductor for photovoltaic applications [10], is very cheap, naturally abundant, and environmentally benign. Indeed, FeS₂ has been used by Energizer in high capacity primary Li/FeS₂ batteries [11] and several groups have recently reported the successful development of rechargeable Li/FeS₂ batteries with excellent electrochemical performance [12–15]. FeS₂ can provide a high theoretical capacity of ~894 mAh/g (based on FeS₂ + 4Na = Fe + 2Na₂S), more than four times higher than the capacity of intercalation-type materials. The high capacity along with the very cheap raw materials makes Na/FeS₂ system a very promising low cost energy storage system. So far, there are only few reports for Na/FeS₂ system in the literature. Almost all of them showed unsatisfactory electrochemical performance with poor reversibility and fast capacity degradation during cycling [16,17]. Recent studies by Okada et al. [18] and Fu et al. [19] indicated that the reaction mechanism between sodium and FeS₂ is complicated and intermediate sodium polysulfide might be involved, as suggested

by Ahn et al. [16] based on the phase diagram of sodium–sulfur. If intermediate sodium polysulfide is generated during the sodiation/desodiation of FeS₂, it is expected to react with carbonate-based electrolyte similar to the reaction between soluble lithium polysulfide and carbonate-based electrolyte via a nucleophilic addition or substitution, which will generate thio-carbonates as nicely demonstrated by Yim et al. [20]. Thus, carbonate-base electrolytes obviously are not a smart choice for Na/FeS₂ system.

Here, for the first time, we demonstrate that by simply substituting ether-based electrolyte for the commonly used carbonate-based electrolyte, the cyclability of FeS₂ towards sodium storage can be significantly enhanced. A sodiation capacity over 600 mAh/g and a discharge energy density higher than 750 Wh/kg can be obtained for FeS₂ at 20 mA/g. When tested at 60 mA/g, FeS₂ presents a sodiation capacity of 530 mAh/g and retains 450 mAh/g after 100 cycles, much better than the cycling performance of Na/FeS₂ tested in carbonate-based electrolyte and the Na/FeS₂ system reported in the literature.

2. Experimental

2.1. Synthesis of FeS₂

FeS₂ was prepared by a two-step method (Fig. 1a). First, Fe₃O₄/carbon composite was synthesized by an aerosol spray pyrolysis method [21]. Briefly, 3.2 g iron (III) nitrate nonahydrate (Fe(NO₃)₃·9H₂O, Sigma-Aldrich) and 6.4 g sucrose (C₁₂H₂₂O₁₁, Sigma-Aldrich) were dissolved into 100 mL distilled water. The solution was nebulized into aerosol droplets, which were carried by argon gas and entered a tubular furnace pre-heated to 700 °C. The sample was collected at the end of the tubular furnace. Second, the Fe₃O₄/carbon composite was mixed with sulfur in a weight ratio of 1:2 and sealed in a glass tube under vacuum condition.

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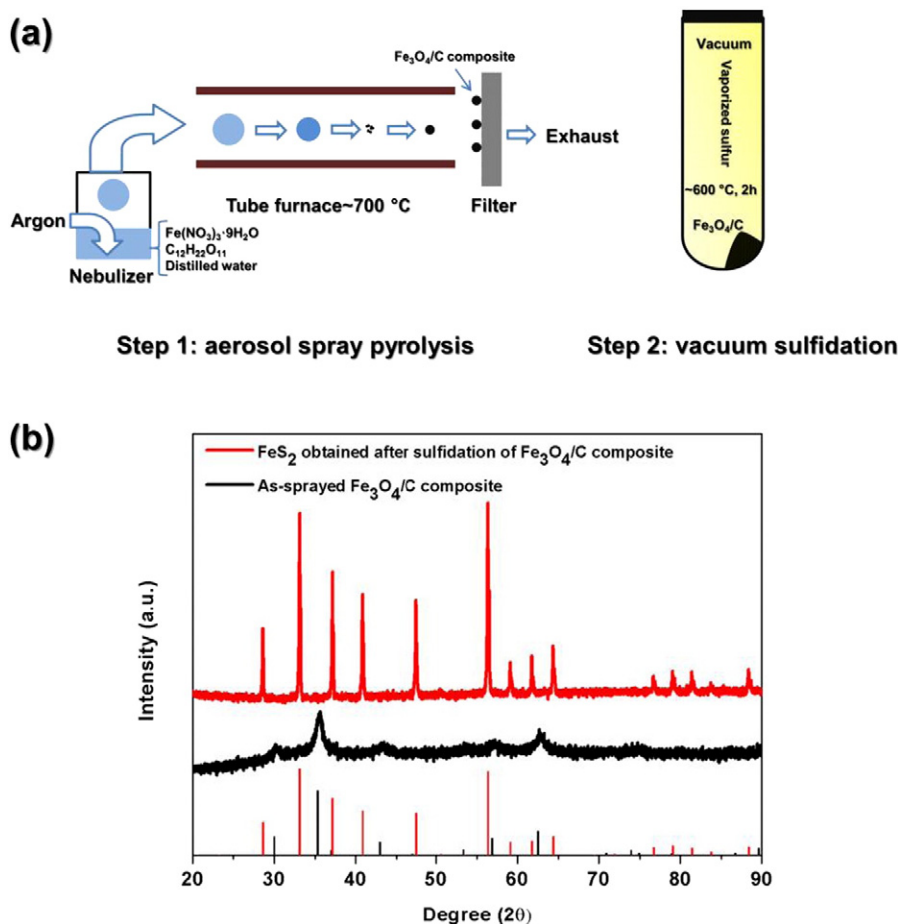


Fig. 1. (a) Schematic illustration of the synthesis process of FeS_2 . (b) XRD patterns of as-sprayed $\text{Fe}_3\text{O}_4/\text{C}$ composite and FeS_2 obtained from vacuum sulfidation of $\text{Fe}_3\text{O}_4/\text{C}$ composite. The standard XRD patterns for Fe_3O_4 (JCPDS card no.: 99-0073) and FeS_2 (JCPDS card no.: 99-0087) are also plotted.

The glass tube was heated to 600°C and held for 2 h. After the glass tube naturally cooled down, the powder was collected and washed with carbon disulfide to remove excess sulfur.

2.2. Material characterizations

The crystal structures of the samples were studied by powder X-ray diffraction (XRD) using a $\text{CuK}\alpha$ radiation source on a D8 Advanced with LynxEye and SolX (Bruker AXS, WI, USA) operated at 40 kV and 40 mA in the 2θ range of 10° – 90° . Scanning electron microscope (SEM) and transmission electron microscope (TEM) were used to investigate the morphologies of the samples.

2.3. Electrochemical tests

The synthesized FeS_2 was manually mixed with sodium alginate binder in water and carbon black in a weight ratio of 85:10:5 to form slurry. Electrode was prepared by coating the slurry onto copper foil with a doctor blade. Then the electrode was dried in a vacuum oven under 100°C for 5 h to remove water. The active material loading on the electrode was about 1.5 – 2.0 mg/cm^2 . CR2032-type coin cells were assembled inside an argon-filled glove box. Sodium foil was used as the counter electrode, Celgard 3501 microporous film was chosen as the separator, and 1.0 M sodium triflate (NaCF_3SO_3 , 98%, Sigma-Aldrich) in diglyme ($(\text{CH}_3\text{OCH}_2\text{CH}_2)_2\text{O}$, anhydrous, 99.5%, Sigma-Aldrich) was selected as the electrolyte for coin cell preparation. For comparison, coin cells with carbonate-based electrolyte (1.0 M NaCF_3SO_3 in ethylene carbonate (EC)/diethyl carbonate (DEC) with a volume ratio of 1:1) were also assembled and tested. Galvanostatic

charge–discharge tests were performed on an Arbin battery test station (BT2000, Arbin Instruments, USA). Coin cells were cycled between 0.6 and 3 V (vs. Na/Na^+) under various current densities. Both current density and specific capacity were calculated on the basis of the weight of as-synthesized FeS_2 in the electrode.

3. Results and discussion

Fig. 1b shows the XRD patterns of the samples. The XRD peak intensity of the as-sprayed material is weak and these peaks can be indexed to Fe_3O_4 , which was generated by incomplete thermal decomposition of $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ under an inert atmosphere. The weak peak intensity indicates a low degree of crystallinity, caused by the rapid heating and cooling during the aerosol spray process. After $\text{Fe}_3\text{O}_4/\text{C}$ reacts with sulfur vapor under vacuum condition, the XRD pattern of the sample can be well indexed to FeS_2 with no crystalline impurity detected.

Fig. 2 shows the SEM and TEM images of $\text{Fe}_3\text{O}_4/\text{C}$ composite and FeS_2 . As shown in Fig. 2a and b, the $\text{Fe}_3\text{O}_4/\text{C}$ composite has a well-defined spherical shape with a diameter around hundreds of nanometers. As evidenced by the contrast difference in the TEM images (Fig. 2c), the $\text{Fe}_3\text{O}_4/\text{C}$ composite has a mesoporous/hollow structure [21]. High resolution TEM image (Fig. 2d) shows that Fe_3O_4 particles with a diameter less than 10 nm are embedded in the carbon matrix. It is hoped that this mesoporous structure could be preserved for FeS_2 , which will be beneficial to its electrochemical performance. However, after sulfidation, the obtained FeS_2 presents an irregular shape (Fig. 2e and f). As shown by the TEM images in Fig. 2g and h, the diameter of the FeS_2 is in the range of 100–600 nm, much larger than that of Fe_3O_4 in the $\text{Fe}_3\text{O}_4/\text{C}$ composite and indicating the

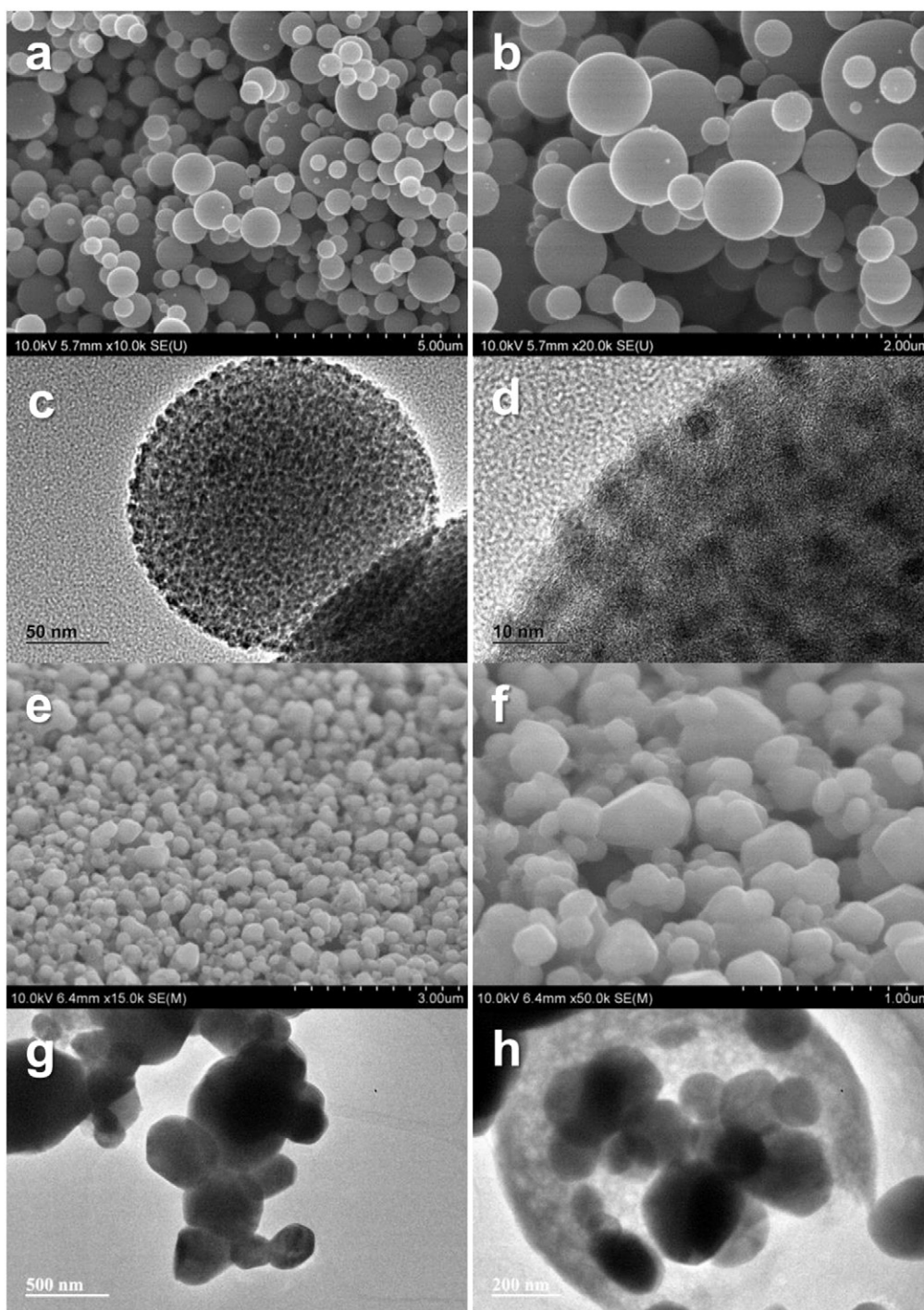
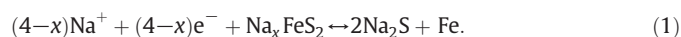


Fig. 2. (a, b) SEM and (c, d) TEM images of as-sprayed $\text{Fe}_3\text{O}_4/\text{carbon}$ composite. (e, f) SEM and (g, h) TEM images of obtained FeS_2 .

aggregation of FeS_2 particles during sulfidation reaction. The particle size of FeS_2 in present study is smaller than that of FeS_2 prepared via mechanical alloying/ball-milling [16,17]. Occasionally, FeS_2 particles encapsulated in carbon shell can be observed during the TEM imaging (Fig. 2h), implying that the mesoporous structure of as-sprayed $\text{Fe}_3\text{O}_4/\text{carbon}$ indeed collapses during the sulfidation reaction.

The electrochemical performance of FeS_2 half-cell with sodium metal as the counter electrode and 1.0 M NaCF_3SO_3 in diglyme as the electrolyte is tested at 20 mA/g. As shown in Fig. 3a, the first sodiation curve is composed of a long plateau around ~1.2 V followed by a sloped line to 0.6 V. The first sodiation capacity is ~670 mAh/g, corresponding to 75% of the theoretical capacity of FeS_2 (894 mAh/g). Subsequent

sodiation profiles show no voltage plateau but sloped shape with higher sodiation voltages in the capacity range of 0–270 mAh/g, considerably different with the first sodiation curve. Recent studies have pointed out that FeS_2 could not be recovered at the end of the first desodiation and a new phase of Na_xFeS_2 was discovered [19], which might account for the observed difference between the first and subsequent sodiation profiles. As suggested by Shadik et al. [19], after the 1st sodiation, the subsequent reversible sodiation–desodiation reaction between FeS_2 and sodium proceeded as following:



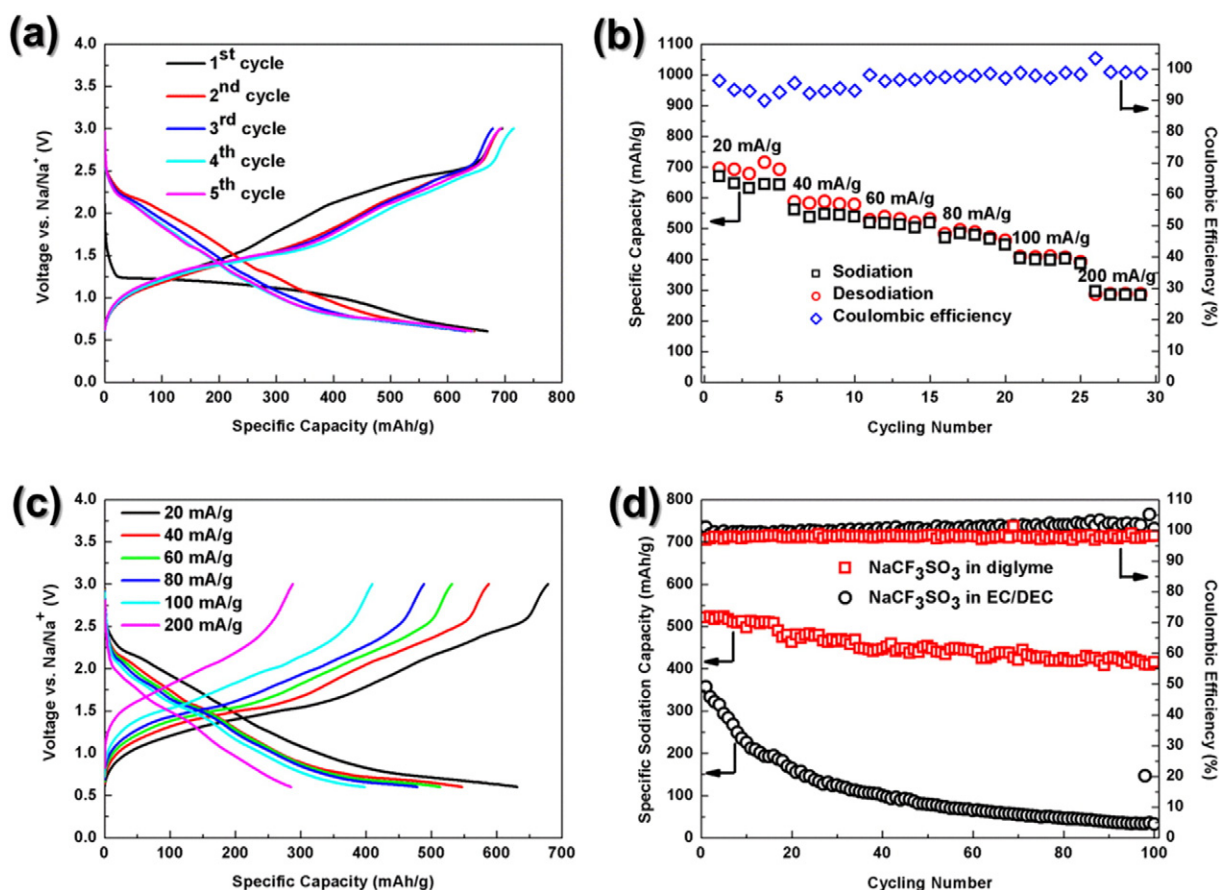


Fig. 3. (a) Initial five sodiation–desodiation voltage profiles of Na/FeS₂ cell tested in 1.0 M NaCF₃SO₃ in diglyme at a current density of 20 mA/g. (b) Sodiation–desodiation capacity and (c) voltage profiles of Na/FeS₂ cycled at various current densities in 1.0 M NaCF₃SO₃ in diglyme. (d) Cycling performance of Na/FeS₂ tested in ether- and carbonate-based electrolytes at 60 mA/g.

The first desodiation profile consists of a sloped curve during the whole process with a capacity of 690 mAh/g. The desodiation profiles during subsequent cycles present similar shape as the first one but lower polarization in the voltage range of 1.5–2.75 V. For the sodiation profiles, the voltage in the 2nd cycle is higher than that of the subsequent cycles. The observed polarization difference between the 1st/2nd cycle and subsequent cycles is probably due to the activation process during the initial few cycles. From the 1st to the 5th cycle, the sodiation and desodiation capacities vary slightly, indicating that the sodiation–desodiation reaction is highly reversible. Although the sodiation voltage of FeS₂ is lower in comparing with intercalation-type cathodes, the Na/FeS₂ system can provide a discharge energy density over 750 Wh/kg at 20 mA/g in the voltage range of 0.6–3 V, much higher than that of intercalation-type materials [9]. The rate capability of Na/FeS₂ system with 1.0 M NaCF₃SO₃ in diglyme electrolyte is shown in Fig. 3b with the corresponding sodiation–desodiation profiles plotted in Fig. 3c. The Na/FeS₂ system can deliver reversible sodiation capacities of 640, 550, 530, 480, 400, and 290 mAh/g at the current densities of 20, 40, 60, 80, 100, and 200 mA/g. The cycling performance of Na/FeS₂ system with 1.0 M NaCF₃SO₃ in diglyme electrolyte is tested at 60 mA/g and the result is shown in Fig. 3d. For comparison, the cycling performance of the same FeS₂ electrode in carbonate-based electrolyte (1.0 M NaCF₃SO₃ in EC/DEC, 1:1 by volume) under the same current density is also tested. The Na/FeS₂ cell tested in carbonate-based electrolyte can provide an initial sodiation capacity of 350 mAh/g. However, the capacity rapidly dropped to less than 40 mAh/g after 100 cycles, similar to the results reported for Na/FeS₂ system in the literature [16,17]. On the contrary, the Na/FeS₂ cell tested in the electrolyte of 1.0 M NaCF₃SO₃ in diglyme demonstrates a high initial sodiation capacity of 530 mAh/g and surprisingly good cyclability with

capacity retention of 415 mAh/g after 100 cycles and Coulombic efficiency (~sodiation capacity/desodiation capacity) over 98% during the whole test, which are much better than the same system tested in carbonate-based electrolyte and the Na/FeS₂ system reported in the literature [16,17]. The improved electrochemical performance of Na/FeS₂ in ether-based electrolyte might be attributed to two factors. First, the application of ether-based electrolyte suppresses the reactions between possible sodium polysulfide and electrolyte. Second, the electrolyte of 1.0 M NaCF₃SO₃ in diglyme avoids the repeated formation and breaking of solid electrolyte interphase (SEI) film since this electrolyte has been shown to be stable in the voltage range of 0.01–3 V (vs. Na/Na⁺) [22].

4. Conclusion

In summary, we demonstrate that by simply selecting ether-based electrolyte (1.0 M NaCF₃SO₃ in diglyme), the cycling performance of Na/FeS₂ system can be greatly improved in comparing with the same system tested in carbonate-based electrolyte (1.0 M NaCF₃SO₃ in EC/DEC). In ether-based electrolyte, the sodium storage capacity in FeS₂ can be over 600 mAh/g with a discharge energy density higher than 750 Wh/kg at 20 mA/g. The Na/FeS₂ cell can be reversibly cycled with sodiation capacity retention of 415 mAh/g after 100 cycles at 60 mA/g. The excellent sodium storage performance and cheap raw materials suggest that Na/FeS₂ system could be a very promising low cost energy storage system as long as the safety issue on the metal anode can be solved in the future. The next step of this work would be the investigation of the exact mechanisms accounting for the significantly improved electrochemical performance of Na/FeS₂ system in ether-based electrolyte.

Conflict of interest

The authors declare no conflict of interests.

Acknowledgments

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